Production Prediction and Optimization Combination in Multilayer Commingled CBM System in Eastern Yunnan and Western Guizhou

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ABSTRACT

The coalbed methane (CBM) reservoirs in eastern Yunnan and western Guizhou have the characteristics of multiple seams superposed, which are commonly exploited by multilayer commingled methods. It is observed that there is crossflow within the reservoir during the development, which impacts the production. To accurately describe the fluid flow law of multilayer CBM co-production, according to the flow mechanism of CBM in composite reservoirs, establish a multilayer combined fluid flow model including crossflow. A numerical simulator based on a fully implicit finite difference solution was developed to analyze the effect of permeability ratio and interlayer pressure differences on production. The results indicate that the numerical simulation results of the established model have a high compliance rate with the fitting results of the field production data, which confirms the validity of the model production prediction in this paper; With the increase of permeability ratio and interlayer pressure difference, the phenomenon of interlayer interference is intensified, the single well production is low, and the degree of reservoir utilization is poor. Differences in the above major influencing factors have resulted in interlayer conflicts and disturbances during combined production. Therefore, the development of CBM reservoirs should select homogeneous multiple coal seams under the same pressure system for coproduction as far as possible. The research results provide a theoretical basis for the rational and efficient development of the CBM reservoir, realize quantitative evaluation of multilayered parameters, and have a certain guiding significance for CBM co-production of the reservoir.

Keywords: coalbed methane, multilayer commingled production, production prediction, interlayer crossflow

NONMENCLATURE

1. INTRODUCTION

CBM is commonly characterized by vertical multilayer stacking due to sedimentation in the formation process [1,2]. For multilayer stacked CBM systems, combined layer drainage can effectively increase the output of a well and reduce the development cost [3]. However, there is the interlayer pressure difference between the reservoirs in the process of discharge and mining, which generates pressure transfer and leads to gas and water crossflow, which has a large impact on the production of CBM wells and is worthy of further study.

Most of the current CBM numerical simulation software focuses on the development of a single coal seam, and there are fewer studies on the fluid flow law of coal-sandstone segments in coal system gas reservoirs

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[4,5]. Aiming at the complexity of the multilayer combined fluid flow problem, Lefkovits [6] established an unstable fluid flow model for multilayer combined reservoirs without considering the interlayer crossflow and derived an analytical solution for the bottom hole flowing pressure. Bourdet [7] developed a theoretical model of multi-reservoir under proposed steady-state flow conditions based on the wellbore reservoir effect and skin factor and plotted the pressure distribution curve. Yonglu Jia [8] derived the solution of the model by Laplace transform based on the multilayer combined mining model established by Bourdet. Jin Huo [9] proposed a mathematical model of fluid flow in a threelayer co-production reservoir with a fixed pressure boundary, obtained the pressure dynamic calculation formula, drew a Dimensionless pressure plate, and analyzed the effect of interlayer crossflow on pressure. Xianmin Zhang [10] constructed a mathematical model of fluid flow from multilayer combined CBM wells and solved the model approximately based on numerical inversion. The majority of existing numerical simulation studies on the production of multilayer CBM wells have focused on interlayer flow problems generated by connecting multiple reservoirs in the wellbore. However, these studies have not considered the crossflow generated by pore connectivity within the adjacent reservoirs, nor have they conducted an in-depth analysis of the change rule of production and its influencing factors.

Therefore, this paper establishes a fluid flow model for coal-sandstone seam mining by introducing the interlayer crossflow, simulates and researches the production law of CBM wells under the multilayer mining method, and clarifies the main controlling factors affecting the gas production of CBM wells, to provide certain references for the multilayer mining of coal strata.

2. METHODOLOGY

2.1 Physical model and assumptions

For CBM reservoirs containing sandstone interbedded layers, combined layer drainage involves multiple scales of mass transfer including desorption, diffusion, fluid flow, and interlayer crossflow [11-16], Wang [1] established a full-process coupled flow model of gas-water two-phase in multi-Coalbed methane reservoirs by comprehensively considering dynamic permeability and crossflow. The physical model is shown in Figure 1.

To facilitate the study, the following basic assumptions are introduced when constructing the three-layer coupled flow model for coal-sandstone seams:

(1) Coal seam is a dual-porosity media containing matrix blocks and fracture networks, and sandstone is a single-porosity system [17-19].

(2) The adsorbed methane is desorbed from the coal matrix surface into the matrix and enters the fractures by diffusion, and the gas adsorption satisfies the Langmuir equation [20-24].

(3) The flow of fluids through the fractures of both coal and sandstone seams is Darcy flow.

(4) Fluid flows between coal and sandstone seams in the form of crossflow.

(5) Neglecting the effect of capillary forces and the dissolution of CBM in water.

(6) The temperature is constant during flow.

Coal seam : \mathbf{I} Sandston Direction of fluid transport Coal seam 2

Fig. 1 Multilayer CBM well fluid flow physical model

2.2 *Mathematical model and solution*

A mathematical model applicable to multilayer collocated mining is established and solved, which concluded that the formation pressure is decreased by drainage, and the methane is desorbed from the matrix and then diffuses into the fracture driven by the concentration gradient, generating fluid exchange with the sandstone layers, and finally entering the wellbore output by fluid flow.

2.2.1 Mathematical modeling

The flow equations in the coal seam fracture are as follows:

$$
\nabla \left[\frac{k^{\sigma} k_{rs}^{\sigma}}{\mu_{s}^{\sigma} B_{s}^{\sigma}} \nabla \left(p_{s}^{\sigma} - \rho_{s}^{\sigma} g H^{c} \right) \right] + \Delta q_{\text{gross}}^{c} + q_{\text{gmf}}^{c} - q_{\text{gwell}}^{c} = \frac{\partial}{\partial t} \left(\frac{S_{s}^{\sigma} \phi^{\sigma}}{B_{s}^{\sigma}} \right) (1)
$$

$$
\nabla \left[\frac{k^{\sigma} k_{rs}^{\sigma}}{\mu_{sr}^{\sigma} B_{sr}^{\sigma}} \nabla \left(p_{s}^{\sigma} - \rho_{s}^{\sigma} g H^{c} \right) \right] + \Delta q_{\text{versas}}^{c} - q_{\text{swell}}^{c} = \frac{\partial}{\partial t} \left(\frac{S_{s}^{\sigma} \phi^{\sigma}}{B_{s}^{\sigma}} \right) (2)
$$

Where the superscript of is the coal fracture system, c is the coal seam; the subscript g is the gas phase, w is the water phase; $\Delta q_{\textit{scross}}^c$ and $\Delta q_{\textit{scross}}^c$ are the crossflow rate of gas and water between the coal seam and sandstone, m 3 /d; $q_{\rm gnr}^{\rm c}$ is the desorption volume of CBM, m 3 /d; $q_{\rm gwell}^{\rm c}$ and $q^c_{\textit{wwell}}$ are the production of gas and water, m³/d.

The gas is mainly in the adsorption state in the coal seam, and during the development process, the gas is gradually desorbed as the pressure decreases. The amount of desorption can be expressed as:

$$
q_{\text{gmf}}^c\Big|^{n+1} = \frac{V_a\Big|^{n} - V_a\Big|^{n+1}}{\triangle t}
$$
 (3)

Where q_{gmf}^c ⁿ⁺¹ is the desorption volume of CBM at time $n+1$, m^3/d ; V_a ^{\mid} is the adsorption volume at time n , \int_{a}^{π} , V_a ^{$\left| \right|$} is the adsorption volume at time *n*+1, m³; Δt is time-varying quantity, d.

The adsorption of gases in the matrix micropores satisfies the Langmuir equation and can be expressed as [25]:

$$
V_{a}|^{n} = \frac{V_{L}p_{s}^{\sigma}|^{n}}{p_{s}^{\sigma}|^{n} + p_{L}}
$$
 (4)

Similarly, the transport equation in the pores of the sandstone layer can be obtained as:

$$
\nabla \left[\frac{k^s k_{\text{sg}}^s}{\mu_s^s B_s^s} \nabla \left(p_s^s - \rho_s^s g H^s \right) \right] + \Delta q_{\text{gcross}}^s - q_{\text{gwell}}^s = \frac{\partial}{\partial t} \left(\frac{S_s^s \phi^s}{B_s^s} \right) \tag{5}
$$

$$
\nabla \left[\frac{k^s k_{\text{rw}}^s}{\mu_w^s B_w^s} \nabla \left(p_w^s - \rho_w^s g H^s \right) \right] + \Delta q_{\text{wcross}}^s - q_{\text{wwell}}^s = \frac{\partial}{\partial t} \left(\frac{S_w^s \phi^s}{B_w^s} \right) \tag{6}
$$

Where the superscript *s* is the sandstone pore system; $\Delta q_{\text{gcross}}^s$ and $\Delta q_{\text{wcross}}^s$ are the crossflow rate of gas and water between the sandstone and coal seam, m³/d; $q_{\textit{gwell}}^s$ and $q_{\tiny{swell}}^s$ are the production of gas and water, m³/d.

Due to the different physical properties of coal and sandstone seams, there is often a pressure difference between the layers [26], and the pressure difference produces material exchange, and the amount of interlayer crossflow is:

$$
\Delta q_{\text{gcross}}^c = -\Delta q_{\text{gcross}}^s = \sigma \frac{k^{cf} k_{\text{g}}^f}{\mu_s^f B_s^f} \left(p_s^{cf} - p_s^s \right) \tag{7}
$$

$$
\Delta q_{\text{wcross}}^c = -\Delta q_{\text{wcross}}^s = \sigma \frac{k^{\sigma} k_{\text{rw}}^{\sigma}}{\mu_w^{\sigma} B_w^{\sigma}} \left(p_w^{\sigma} - p_w^s \right) \tag{8}
$$

Where $\sigma = \frac{4}{h^2}$ $\sigma = \frac{4}{h^2}$ is the geometric factor, m⁻².

In order to completely describe the transport process of gas and water and to solve equations, it is also necessary to introduce auxiliary equations and definite conditions.

$$
\begin{cases}\n q_{well} = \frac{\sqrt{k_x k_y} k_r}{\mu B} \frac{2\pi h}{\ln(r_e/r_w) + s} (p - p_{wf}) \\
\frac{\partial p}{\partial x}\Big|_{x=0, L} = 0 \\
\frac{\partial p}{\partial y}\Big|_{y=0, W} = 0 \\
\frac{\partial p}{\partial z}\Big|_{z=0, H} = 0 \\
p(x, y, z, t)\Big|_{t=0} = p_0(x, y, z) \\
S(x, y, z, t)\Big|_{t=0} = S_0(x, y, z)\n\end{cases}
$$
\n(9)

The calculation of r_e introduces the concept of effective wellbore diameter defined by Peaceman:

$$
r_e = 0.28 \frac{\left[\left(k_y / k_x \right)^{0.5} \Delta x^2 + \left(k_x / k_y \right)^{0.5} \Delta y^2 \right]^{0.5}}{\left(k_y / k_x \right)^{0.25} + \left(k_x / k_y \right)^{0.25}}
$$
(10)

Where k_x and k_y are the directional permeability of x and y, mD; Δx and Δy are the mesh size in x and y direction, m.

2.2.2 Solution of the mathematical model

The gas-water two-phase full-process coupled flow model developed above is a complex set of nonlinear partial differential equations. Based on this, the established mathematical model needs to be finite difference processed.

Taking the gas-phase flow equation in a coal seam as an example, a finite difference discretization of Eq. (1) is performed, where the superscript *cf* is omitted and the difference subscripts are in an abbreviated form in the processing, e.g. $i + \frac{1}{2} = i + \frac{1}{2}, j, k$.

Fig. 2 Flowchart of the CBM simulator

Define the specific weight, mobility, conduction coefficient, and second-order difference quotient operators as shown in Eq. (11), (12), (13), and (14):

 $\sqrt{ }$

$$
\gamma_s = \rho_s g \tag{11}
$$

$$
\lambda_{g} = \frac{k k_{r_{g}}}{\mu_{g} B_{g}}
$$
 (12)

$$
T_{xg\left(i+\frac{1}{2}\right)} = \frac{\Delta y_j \Delta z_k}{\Delta x_{i+\frac{1}{2}}} \lambda_{g\left(i+\frac{1}{2}\right)}, \quad T_{xg\left(i-\frac{1}{2}\right)} = \frac{\Delta y_j \Delta z_k}{\Delta x_{i-\frac{1}{2}}} \lambda_{g\left(i-\frac{1}{2}\right)}
$$
\n
$$
T_{yg\left(j+\frac{1}{2}\right)} = \frac{\Delta x_i \Delta z_k}{\Delta y_{j+\frac{1}{2}}} \lambda_{g\left(j+\frac{1}{2}\right)}, \quad T_{yg\left(j-\frac{1}{2}\right)} = \frac{\Delta x_i \Delta z_k}{\Delta y_{j-\frac{1}{2}}} \lambda_{g\left(j-\frac{1}{2}\right)} \tag{13}
$$
\n
$$
T_{xg\left(k+\frac{1}{2}\right)} = \frac{\Delta x_i \Delta y_j}{\Delta z_{k+\frac{1}{2}}} \lambda_{g\left(k+\frac{1}{2}\right)}, \quad T_{xg\left(k-\frac{1}{2}\right)} = \frac{\Delta x_i \Delta y_j}{\Delta z_{k+\frac{1}{2}}} \lambda_{g\left(k-\frac{1}{2}\right)} \tag{14}
$$
\n
$$
\lambda_x T_{xg} \Delta_x P_g = T_{xg\left(i+\frac{1}{2}\right)} \left(P_{g\left(i+1} - P_{g\left(i\right)} \right) - T_{xg\left(i-\frac{1}{2}\right)} \left(P_{g\left(i-1} - P_{g\left(i\right)} \right) \right)
$$
\n
$$
\Delta_y T_{yg} \Delta_y P_g = T_{yg\left(j+\frac{1}{2}\right)} \left(P_{g\left(i+1} - P_{g\left(i\right)} \right) - T_{yg\left(j-\frac{1}{2}\right)} \left(P_{g\left(i-1} - P_{g\left(i\right)} \right) \right) \tag{14}
$$
\n
$$
\Delta_z T_{zg} \Delta_z P_g = T_{zg\left(k+\frac{1}{2}\right)} \left(P_{g\left(k+1} - P_{g\left(k\right)} \right) - T_{zg\left(k-\frac{1}{2}\right)} \left(P_{g\left(k-1} - P_{g\left(k\right)} \right) \right)
$$

Using block centered grid system, the difference equation for the point $(i, j, k, n+1)$ is:

$$
\Delta_x T_{xg} \Delta_x p_g \Big|^{n+1} + \Delta_y T_{yg} \Delta_y p_g \Big|^{n+1} + \Delta_z T_{zg} \Delta_z p_g \Big|^{n+1}
$$
\nreliability of the sir
\n
$$
-\Delta_x T_{xg} \gamma_g \Delta_x H^c - \Delta_y T_{yg} \gamma_g \Delta_y H^c - \Delta_z T_{zg} \gamma_g \Delta_z H^c
$$
\n
$$
+ \Delta q_{gcross} V_{ijk} + q_{gmf} V_{ijk} - q_{gwell} V_{ijk} = \frac{V_{ijk}}{\Delta t} \Bigg[\Bigg(\frac{S_g \phi}{B_g} \Bigg)^{n+1} - \Bigg(\frac{S_g \phi}{B_g} \Bigg)^n \Bigg] \Bigg]
$$
\n(15) Figure 4 illustrate crossflow is su
\nLHS
\nTable 1 Simplitor validation of input parameters

Define again as follows:

$$
\Delta T_{g} \Delta p_{g} \Big|^{n+1} = \Delta_{x} T_{xg} \Delta_{x} p_{g} \Big|^{n+1} + \Delta_{y} T_{yg} \Delta_{y} p_{g} \Big|^{n+1} + \Delta_{z} T_{zg} \Delta_{z} p_{g} \Big|^{n+1} \quad (16)
$$

$$
\Delta T_{g}\gamma_{g}\Delta H^{c} = \Delta_{x}T_{xg}\gamma_{g}\Delta_{x}H^{c} + \Delta_{y}T_{yg}\gamma_{g}\Delta_{y}H^{c} + \Delta_{z}T_{zg}\gamma_{g}\Delta_{z}H^{c}
$$
 (17)

$$
Q = \Delta q_{\text{gcross}} + q_{\text{gmf}} - q_{\text{gwell}} \tag{18}
$$

Eq. (15) can be simplified as:

$$
\Delta T_{g} \Delta p_{g} \Big|^{n+1} - \Delta T_{g} \gamma_{g} \Delta H^{c} + Q V_{ijk} = \frac{V_{ijk}}{\Delta t} \left[\left(\frac{S_{g} \phi}{B_{g}} \right)^{n+1} - \left(\frac{S_{g} \phi}{B_{g}} \right)^{n} \right] \tag{19}
$$

The Newton-Raphson iterative fully implicit equations are used to solve the above discrete equations to obtain a multilayer commingled simulator for CBM reservoirs. The schematic of the simulator solution is shown in Figure 2.

3. MODEL AND ALGORITHM VALIDATION

The reliability of the mathematical model and simulator is verified by comparing and analyzing the actual production data. The input parameters of the simulator are shown in Table 1. The comparison results of CBM production are shown in Figure 3, and the simulator calculation results have good consistency with the production data, which preliminarily verifies the reliability of the simulator.

Figure 4 illustrates that the production considering crossflow is smaller than ignoring crossflow. Furthermore, the longer the time, the larger the difference between the two.

Fig. 3 Comparison of field data and simulation results

Fig. 4 Cumulative gas production curve considering/ignoring interlayer crossflow

After 120 days, the cumulative production decreased by 25 %, which can be attributed to the higher permeability of the coal seam compared to that of the sandstone. This results in the gas flowing from the sandstone to the coal seam, reducing the pressure drop within the coal seam. Consequently, the interlayer crossflow cannot be disregarded when conducting a prediction of the CBM production.

4. ANALYSIS OF INFLUENCING FACTORS

Two important factors affecting the combined production, permeability ratio, and reservoir pressure

Permeability/mD				Pressure/MPa			
Coal seam 1	Sandstone	Coal seam 2	m	Coal seam 1	Sandstone	Coal seam 2	n
0.5	0.02	0.5			9.5	10	0.5
0.8	0.02	0.2				10	
0.9	0.02	0.1	q		8.5	10	

Table 2 Parameter values for sensitivity analysis

4.1 Effect of permeability ratio

In order to study the effect of reservoir inhomogeneity on gas well production, a combined mining model was established by considering the permeability ratio of the main producing seams (Coal seam 1 and Coal seam 2) to be 1, 4, and 9, respectively, while ensuring the same average permeability.

Fig. 5 Cumulative gas production curves with different permeability ratio

As can be seen from Figure 5, in the early stage of production, the permeability ratio has less influence on fluid flow, which is because at this time, coal seam 1 is the main production layer, and the production is affected by the permeability of a single layer. As the gas reservoir pressure gradually decreases to the critical desorption pressure, the adsorbed gas in the coal seam begins to desorb, resulting in an upward curve of cumulative production. The contribution of coal seam 2 to the production begins to appear, and the cumulative production of gas wells decreases with the increase of permeability ratio, and the phenomenon of interlayer interference increases.

In order to further analyze the result, the plan view of the pressure distribution of coal seam 1, sandstone and coal seam 2 at the discharge time of 1000d was plotted. Comparing the results of pressure drop funnels of coal seam 1 under different permeability ratio, it can be seen that with the increase of permeability ratio, the initial permeability of coal seam 1 is larger, the pressure

drop transfer rate of this layer is faster, the transfer range is larger, and it is easy to form deeper pressure drop funnels at the wellbore, which leads to the increase of gas production from this layer.

However, as the permeability of coal seam 1 increases, the pressure drop of coal seam 2 reservoir is

difference, were selected as research objects for sensitivity analysis, and the specific parameter settings are shown in Table 2.

Permeability ratio m refers to the ratio of the maximum permeability to the minimum permeability of the main producing seams (Coal seam 1 and Coal seam 2), and reservoir pressure difference n refers to the difference in pressure between adjacent seams.

$$
m = \frac{k_{\text{max}}}{k_{\text{min}}} \qquad n = p_{down} - p_{up} \tag{20}
$$

smaller, and the pressure drop funnel becomes more difficult to expand. This is because under the condition of certain drainage, with the increase of permeability of

Fig. 7 Variation of pressure in coal seam 2 with different permeability ratio (Time=1000d)

Fig. 8 Variation of pressure in sandstone with different permeability ratio (Time=1000d)

coal seam 1, the drainage in the layer increases, which leads to the decrease of drainage in the adjacent layer, the pressure drop is smaller, and the production capacity is suppressed, thus causing the total gas production to decrease. Meanwhile, as the sandstone layer is a lowpermeability section, the permeability grade difference has little effect on the low-permeability section, and the pressure drop funnel is almost unchanged.

In summary, the permeability ratio mainly affects the combined production capacity through pressure drop. The initial permeability has a positive effect on the production capacity of this layer, which is manifested in the fact that the larger the permeability is, the larger the single-layer production is. However, the initial permeability has an inhibitory effect on the neighboring layers, and the larger the permeability is, the more obvious the inhibitory effect is, thus causing the total production capacity to decline. Therefore, the existence of interlayer interference phenomenon should be considered in the development process, and the combination of layers with the same physical properties should be mined as far as possible.

In order to quantitatively analyze the degree of interlayer interference in multi-layer combined mining in CBM reservoirs, the single mining index Ji, the combined mining index J, and the dimensionless interlayer interference coefficient λ are defined, respectively.

$$
J_{i} = \frac{Q_{sgi}}{p_{ei} - p_{wfi}} \qquad J = \sum_{i=1}^{3} \frac{Q_{cgi}}{p_{ei} - p_{wfi}}
$$
(21)

$$
\lambda = \frac{J}{\sum_{i=1}^{3} J_i}
$$
 (22)

Where the $Q_{\text{sg}i}$ is the gas production when the layer is extracted alone, m^3/d ; the Q_{cgi} is the gas production when the layers are extracted together e, m^3/d .

The interlayer interference coefficient describes the degree of release of gas recovery capacity of multi-layer gas wells, and the smaller its value, the more serious the interlayer interference phenomenon. In this study, 0.5 is used as the limit of interlayer interference in multi-layer gas extraction, less than this value indicates that the interlayer conflict is prominent and unsuitable for coexploitation and development.

Fig. 9 Variation of interlayer interference coefficient with different permeability ratio

The change of interlayer interference coefficient with production time under different permeability ratio is shown in Fig. 9, which shows that the interlayer interference coefficient decreases with the increase of production time, and the larger the permeability ratio is, the more serious the interlayer interference is. Overall, in the late production period, when the permeability ratio is 1, the interlayer interference coefficient is stable

near 0.9, which is suitable for co-mining and development; when the permeability ratio is 4, the interlayer interference coefficient decreases to 0.7, which needs to be considered comprehensively at this time; when the permeability ratio is 9, the interlayer interference coefficient decreases rapidly, and stabilizes at the late stage near 0.45, which is not suitable for comining and development.

4.2 Effect of reservoir pressure difference

For multilayer continuous reservoir formation, the pressure systems of neighboring layers are not equal. During the mining process, interlayer interference occurs between high-pressure coal seams and low-pressure coal seams through sandstone interbedding, so the effect of different reservoir pressure differences on gas well production is investigated.

Fig. 10 Cumulative gas production curves with different reservoir pressure difference

As can be seen from Figure 10, in the early stage of production, the influence of interlayer pressure difference on the cumulative gas production is not obvious, which is because at this time, coal seam 1 is the main production layer, and the interlayer interference phenomenon is not yet significant. As production proceeds, the inhibitory effect of the high-pressure coal seam on the low-pressure coal seam is strengthened, and the cumulative production of the gas wells decreases with the increase of the reservoir pressure difference, and the phenomenon f inter-stratum interference is intensified.

Reservoir pressure characterizes the level of energy and also determines the difficulty of development. The smaller the interlayer pressure difference is, the larger the initial pressure of coal seam 1 is. Fig. 11 shows the change of pressure drop of coal seam 1 under different interlayer pressure difference conditions during 1000d of production, which shows that with the increase of initial pressure, the pressure drop funnel is expanding and deepening, which has a promoting effect on the production capacity of this segment.

As coal seam 1 continues to be extracted, the pressure difference between adjacent segments will be more significant, which is manifested in the increase of gas production from coal seam 2. Meanwhile, as the sandstone layer is a low-permeability layer section, the pressure drop funnel changes little.

Fig. 11 Variation of pressure in coal seam 1 with different pressure difference (Time=1000d)

Fig. 12 Variation of pressure in coal seam 2 with different pressure difference (Time=1000d)

In summary, the reservoir pressure difference mainly affects the pressure of coal seam 1. The smaller the interlayer pressure difference is, the reservoir pressure of the first seam section gradually increases, which promotes the total production. Therefore, the size of the interlayer pressure difference should be considered in the process of multi-gas mining, and the gas-bearing layers in the same pressure system should be mined as far as possible.

The change of interference coefficient with production time under different interlayer pressure

differences is shown in Figure 14, which shows that the interlayer interference coefficient decreases with the increase of production time, and the larger the interlayer differential pressure is, the more serious the interlayer interference is. When the interlayer pressure difference is 0.5, 1 and 1.5 MPa, the interlayer interference coefficients are 0.88, 0.8, and 0.7, respectively.

Fig. 13 Variation of pressure in sandstone with different pressure difference (Time=1000d)

5. CONCLUSIONS

The interlayer crossflow was introduced to establish a multilayer combined mining fluid flow model for CBM reservoirs, and the reliability of the model was verified by comparing it with examples, and the relationship between the permeability ratio and reservoir pressure difference and the production of the combined wells was investigated respectively, and the conclusions obtained are as follows.

(1) A mathematical model of fluid flow in multilayer combined CBM reservoirs was constructed, and a numerical simulator based on the finite-difference method was developed, which was verified by comparing with well data to achieve an accurate characterization of fluid transport in multilayer combined CBM reservoirs.

(2) For heterogeneous reservoirs, the influence of heterogeneity on the production of joint extraction wells cannot be ignored. Under the condition of the same average permeability, the larger the permeability ratio, the smaller the yield, the more intense the interlayer interference, and the worse the degree of reservoir mobilization. Permeability ratio is proportional to the intensity of interference, permeability ratio is greater than 9, the interlayer interference coefficient is reduced to less than 0.5, which is not suitable for co-mining and development.

(3) For composite reservoirs, the interlayer pressure difference causes fluid transport between different reservoirs, the larger the interlayer pressure difference, the smaller the yield, and the degree of interlayer interference is intensified, so it is recommended to select multiple coal seams with the same pressure system for combined mining. The interlayer pressure difference is positively proportional to the interference intensity, and the interlayer pressure difference is within 1MPa, which is suitable for co-mining and development.

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DECLARATION OF INTEREST STATEMENT

The authors declare that they have no known competing financial interests or personal relationships that could have an impact on the work reported in this paper.

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